

### **LISTING OF CLAIMS**

1. (Original) Process for preparation of middle distillates by selective conversion of a hydrocarbon containing feedstock under hydrocracking conditions with a hydrocarbon conversion catalyst comprising one or more hydrogenation components supported on a support comprising a beta zeolite and an amorphous inorganic oxide, the beta zeolite having a SiO<sub>2</sub>: Al<sub>2</sub>O<sub>3</sub> molar ratio of at least 50, and the amorphous inorganic oxide consisting of silica-alumina and alumina and combinations thereof, the support having an Ion Exchange Capacity-Acidity Index of less than 3.7.
2. (Original) Process of claim 1 wherein the support has an NH<sub>3</sub>-TPD Acidity Index of less than 3.5.
3. (Previously presented) Process of claim 1, in which the NH<sub>3</sub>-TPD Acidity Index is less than 2.3 and/or the Ion Exchange Capacity-Acidity Index is less than 2.7.
4. (Original) Process of claim 1, wherein the beta zeolite has a SiO<sub>2</sub>: Al<sub>2</sub>O<sub>3</sub> molar ratio of at least 100.
5. (Original) Process of claim 1, wherein the one or more hydrogenation components are selected from the elements of Group VIII and/or Group VI B.
6. (Original) Process of claim 5, wherein the hydrogenation components are selected from the group consisting of tungsten, molybdenum, nickel and combinations thereof.
7. (Original) Process of claim 6, wherein the hydrogenation components are a combination of nickel and tungsten.
8. (Original) Process of claim 1, wherein the support comprises less than 50 wt %

zeolite beta and at least 50 wt % amorphous inorganic oxide.

Claims 9-10. (Canceled)

11. (Previously presented) Process of claim 2, in which the  $\text{NH}_3$ -TPD Acidity Index is less than 2.3 and/or the Ion Exchange Capacity-Acidity Index is less than 2.7.